

# Comparison ability of algae and nanoparticles on nitrate and phosphate removal from aquaculture wastewater

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## Abstract

**Background:** Aquaculture wastewater contains high levels of phosphate and nitrate. The reuse of this water requires standards beyond the secondary standards to eliminate more organic pollutants from aquaculture effluents. In this research, the removal of these pollutants from wastewater using *Chlorella vulgaris* and  $Fe_3O_4$  nanoparticles in the reactor space was investigated.

**Methods:** This study was conducted on fish farms effluent in the laboratory system. For this purpose, a 5-L semi-industrial reactor with a mixer blade, porous plate, and a compressor was designed. *Chlorella vulgaris* samples were collected from the natural environment and cultured in the laboratory environment. Also,  $Fe_3O_4$  nanoparticles were prepared from Iranian Nano Pishgaman Company to make the desired solution. During the experiment (3 weeks), samples were taken weekly (in one phase) from the effluent. Dissolved oxygen (DO), pH, nitrate ( $NO_3$ ), and phosphate ( $PO_4$ ) factors from the influent and effluent of the farms were measured. The statistical data were analyzed using SPSS version 21 and Excel 2013.

**Results:** The amounts of nitrate and phosphate were decreased by about 80.76 and 80.55% in the biological reactor, whereas these amounts were 70.52 and 70.48% in the nanoparticle reactor, respectively. Also, there were significant differences in the amounts of  $NO_3$  and  $PO_4$  between the control treatment and weekly treatment ( $P < 0.05$ ).

**Conclusion:** Based on the results, both reactors were able to reduce nitrate and phosphate from aquaculture wastewater, but the efficiency of the biological reactor was higher than that of the nanoparticle reactor.

**Keywords:** Nitrate, Phosphate,  $Fe_3O_4$  nanoparticle, *Chlorella vulgaris*, Biological refinement

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## Introduction

Sewage production has been grown dramatically with increasing population growth, water consumption, and industrial development. The discharge of sewage causes environmental degradation, contamination of surface waters and underground resources, and the occurrence of acute and chronic diseases (1,2). Nitrogen and phosphate are essential elements for plants and living organisms. Nonetheless, the entry of nitrogen and nitrogen from agricultural land, untreated municipal, and industrial wastewaters into the water can be one of the most important sources threatening water quality (3). Algae have the ability to absorb nitrogen and

phosphate nutrients for photosynthesis, pigment and protein production. Algae are capable of absorption of nutrients even at low concentrations due to resistance to temperature and pH changes. Also, algae have simple and inexpensive production technology (4). The excessive growth of the aquaculture industry through the excessive use of natural resources has disrupted natural balance. The aquaculture effluents can be as a source of pollution in the environment (5).

The studies have shown that low levels of nitrogen (about  $0.4 \text{ mg L}^{-1}$ ) and phosphorus (about  $0.1 \text{ mg L}^{-1}$ ) in calm waters (i.e., swamps and lakes) cause rapid growth of algae (6,7). Therefore, their growth reduces the concentration



of dissolved oxygen and the penetration of light into the water, which leads to the destruction of fish and microorganisms. By the death of these organisms, the oxygen demand for their decomposition increases. In these conditions, the aerobic environment becomes anaerobic and all of these processes lead to water enrichment. In addition to the problems caused by this phenomenon for the environment, the process of purifying these waters is costly and undesirable (6,7). Drinking Nitrate-contaminated water causes children's blood diseases and adults' gastro-intestinal cancers. Therefore, the level of phosphate and nitrogen must be reduced prior to the discharge of effluent into the aquatic environments (8). There is a wide range of sewage treatment systems that often have some limitations, such as high cost and high energy consumption, which often require complex maintenance and operation but also have high efficiency, including biodegradation (9).

Nowadays, nanoparticles are also used to remove pollutants. Various studies have suggested the effectiveness of this method in removing pollutants such as heavy metal cations and nitrate compounds (10). There are various physical, chemical, and biological methods to reduce the amount of effluents from the aquaculture in the environment and soil (11). A lot of studies have been done to determine the effect of aquaculture wastewaters on the environment and also to find pollution control ways (12-17). Although physical and chemical methods may be effective, these methods are costly and do not result in complete decomposition or complete destruction of the contaminants. In the biodegradation method, pollutants are consumed by micro-algae as food and turned into biological cells or living masses, and finally, are removed from the environment. Due to the problems caused by phosphates, nitrates, and other pollutants in the drinking waters and the enrichment of water resources, the aim of this study was to reduce the nutrients of aquaculture effluents discharged in the environment using biological and nanoparticle reactors in the laboratory environment.

## Materials and Methods

### Microalgal culture

*Chlorella vulgaris* samples were collected from the natural environment and cultured under laboratory conditions. The continuous light and temperature were  $50 \mu\text{mol photons m}^{-2} \text{s}^{-1}$  and  $25^\circ\text{C}$ , respectively. An artificial culture environment was used to cultivate algae. The artificial culture environment contained  $\text{NaNO}_3$ ,  $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$  (2.94 mM),  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$  (0.05 mM),  $\text{K}_2\text{HPO}_4$  (0.30 mM),  $\text{KH}_2\text{PO}_4$  (0.17 mM),  $\text{NaCl}$  (0.43 mM), and  $\text{CaCO}_3$  (1.29 mM). Other micronutrients were prepared according to the BG11 culture medium (18). *C. vulgaris* was cultured in a volume of 100 mL in a 250 ml Erlenmeyer in a micronutrient-enriched artificial culture environment. The algae cultivation was continued for 10 days. The required light was supplied with a high radiation

fluorescent lamp and the cultures were stirred at a speed of 150 rpm. The light was measured and adjusted using a 1339 Lux meter. This method was continued to provide a suitable density and volume of the algae stoke. Then, the algae were added to the reactor space containing wastewater from fish farms.

### Preparation of iron oxide nanoparticles stock

Iron oxide nanoparticle (NPs, with a diameter of 40 nm, purity of 99%, US Research Nanomaterials, Inc) was prepared from Iranian Nano Pishgaman Company to make a favorite solution. The nanoparticles were dispersed for 40 minutes using an ultrasound machine with a stirring rate of 400 rpm in the distilled water (250 cc) to homogenize. Since iron nanoparticles may be deposited on the bottom of the reactor, a stirrer engine was used to disperse nanoparticles in the water environment. Also, the water samples were tested by dynamic light scattering (DLS) technique to determine the dispersion rate of nanoparticles in the mixing tank.

### Preparation of wastewater samples

All wastewater samples were collected from the fish farms of Shahid Rajai center located in the suburb of Sari city ( $36^\circ 37' 0'' \text{ N}$ ,  $53^\circ 8' 58'' \text{ E}$ ), Mazandaran province. The main target of this center is the production of the fish larva (bony fish and sturgeon larvae) for the sustainable development of aquatic animals.

### Reactor design

To design a semi-industrial reactor in an unconstrained mode, the reactor volume was optionally set at 5 L and design calculations were performed (Figure 1). The reactor can be designed according to the standard dimensions for reservoir reactors (19).

Proportions in the construction of the reactor dimensions were ( $D = H_L$ ), ( $d = H_i$ ), ( $d/D = 1/3$ ), ( $L/d = 1/4$ ), and ( $b/d = 1/5$ ). According to the present standard, the dimensions of a 5 L semi-industrial reactor would be as follows: ( $H_L = 20.5 \text{ cm}$ ), ( $D = H_L = 20.5 \text{ cm}$ ), ( $d = H_i = 6.83 \text{ cm}$ ), ( $b = 1.366 \text{ cm}$ ), ( $L = 1.7 \text{ cm}$ ), and ( $W_b = 1.43 \text{ cm}$ ).

### The mixer used for designed reactor

Homogenization of nanoparticles and algae was performed

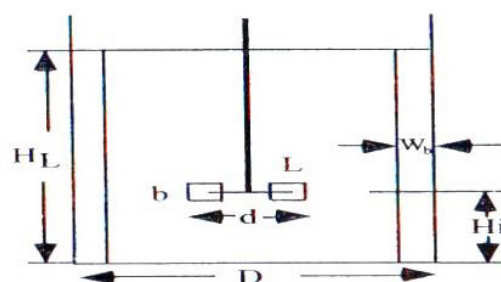


Figure 1. Standard dimensions of reservoir reactor (19).

using a homogenizer with a speed of 14000 rpm in the laboratory. In order to provide suitable conditions for the 5-liter bioreactor, the mixer was designed as a turbine and its dimensions are presented in Figure 2.

According to the requirements of the reaction, the standard for the reactor, and blade dimensions, the ratio of blade diameter to the turbine blade tank diameter is 0.3 to 0.5 (20). Therefore, a suitable blade was selected for the turbine of the designed bioreactor. The required power was the most important parameter for the designed mixer, which was calculated using Eq. 1 (21):

$$P_A = P_0 \rho N^3 D_A^5 \quad (1)$$

where  $P_0$  is the air column pressure,  $\rho$  is density,  $N$  is the length of flow,  $D$  is the depth of flow, and  $\mu$  is the viscosity of flow.  $P_0$  was calculated by the mixing Reynolds number. The Reynolds number was calculated using Eq. 2 (21):

$$Re_M = \frac{\rho N D_A^2}{\mu} = \frac{(1000 \times 2.167 \times (0.0683^2))}{0.1} = 101.09 \quad (2)$$

In order to prevent the nanoparticles deposition at the bottom of the reactor, a porous plate with an air inlet is required to create turbulence in the reservoir (Figure 3). Therefore, the air was transferred to the lower surface of the reactor using a compressor (by a tube with a diameter of 1/8 inch) (Figure).

The fluid pressure inside the bioreactor was calculated using Eq. 3 (21):

$$P = \rho gh + p_0 = 1000 \times 9.8 \times 0.1435 / 101325 + 1 = 1.014 \text{ atm} \quad (3)$$

where  $P_0$  is the air column pressure,  $\rho$  is density,  $G$  is the gravitational acceleration, and  $h$  is the liquid column height.

Nitrate and phosphate were measured by a Nanocolor spectrophotometer (UV-Vis Spec, Germany). Also, pH and DO parameters were measured by the 780 pH Meter (Metrohm, Sweden) and D.O. meter (AZ8403), respectively (22). The statistical data were analyzed using SPSS version 21 and Excel 2013.

## Results

The amounts (mean  $\pm$  SE) of  $\text{NO}_3^-$ ,  $\text{PO}_4^{3-}$ , DO, and pH measured during the experiment for nanoparticle and biological reactors are presented in Tables 1 and 2, respectively. In the nanoparticle reactor, the concentration of nitrate was  $48.61 \pm 7.2 \text{ mg L}^{-1}$  in the control treatment but it was decreased to  $16.01 \pm 9.6 \text{ mg L}^{-1}$  after three weeks. Also, the concentration of phosphate in the control treatment was  $8.52 \pm 1.27 \text{ mg L}^{-1}$  but it was decreased to  $2.86 \pm 0.47 \text{ mg L}^{-1}$  after three weeks. The amounts of DO and pH in the control treatment were  $5.17 \pm 2.18 \text{ mg L}^{-1}$  and  $8.69 \pm 0.1$  treatment, respectively, while these amounts decreased to  $4.83 \pm 1.62 \text{ mg L}^{-1}$  and  $8.73 \pm 0.19$  in the third week of treatment, respectively. There were significant

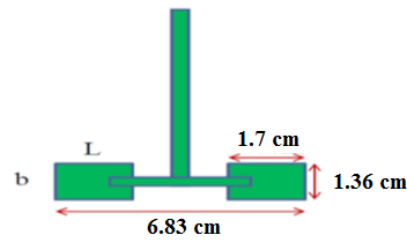


Figure 2. Schematic of the designed mixer in the reactor.

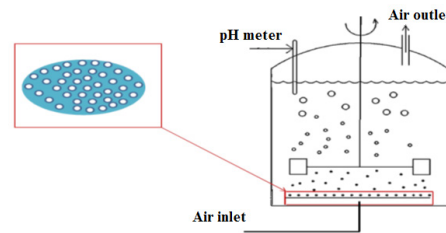


Figure 3. A schematic of air injection to the bioreactor and penetration in the fluid.

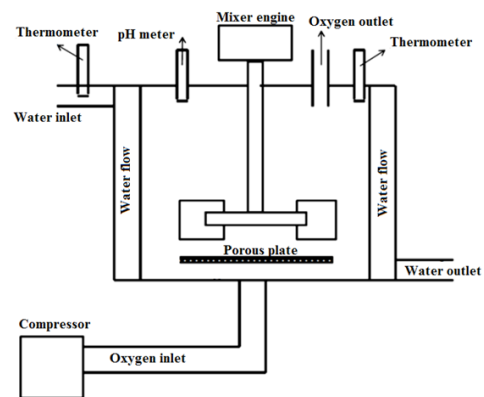


Figure 4. A complete schematic of the designed reactor.

differences in the amounts of  $\text{NO}_3^-$ ,  $\text{PO}_4^{3-}$ , and DO between the control treatment and weekly treatments ( $P < 0.05$ ) (Table 1).

In the biological reactor, the amount of nitrate in the control treatment was  $48.61 \pm 7.2 \text{ mg L}^{-1}$  but it was decreased to  $24.53 \pm 5.61 \text{ mg L}^{-1}$  after three weeks. Also, the amount of phosphate in the control treatment was  $8.52 \pm 1.27 \text{ mg L}^{-1}$  but it was decreased to  $4.34 \pm 0.39 \text{ mg L}^{-1}$  after three weeks. The amounts of DO and pH in the control treatment were  $5.17 \pm 2.18 \text{ mg L}^{-1}$  and  $8.69 \pm 0.1$  whereas these amounts decreased to  $4.57 \pm 1.27 \text{ mg L}^{-1}$  and  $8.57 \pm 0.26$  after three weeks, respectively. There were significant differences in the amounts of  $\text{NO}_3^-$ ,  $\text{PO}_4^{3-}$ , and DO between the control treatment and weekly treatments ( $P < 0.05$ ) (Table 2).

The results of comparison of the nitrate and phosphate changes among wastewater inlet, control treatment, and weekly treatments in the nanoparticle and biological reactors are presented in Figures 5 and 6. According to the

**Table 1.** The measured amounts (mean ± SE) of parameters in the inlet and outlet of the nanoparticle reactor during the experiment

Parameter	Wastewater inlet	Outlet (First week)	Outlet (Second week)	Outlet (Third week)	Control treatment
NO3 (mg L <sup>-1</sup> )	83.2	21.43±9.9 <sup>b</sup>	18.61±6.2 <sup>c</sup>	16.01±9.6 <sup>c</sup>	48.61±7.2 <sup>a</sup>
PO4 (mg L <sup>-1</sup> )	14.7	3.21±0.42 <sup>b</sup>	3.07±0.31 <sup>b</sup>	2.86±0.47 <sup>c</sup>	8.52±1.27 <sup>a</sup>
DO (mg L <sup>-1</sup> )	1.27	4.47±1.09 <sup>b</sup>	4.61±1.07 <sup>b</sup>	4.83±1.62 <sup>b</sup>	5.17±2.18 <sup>a</sup>
pH	7.58	8.51±0.1 <sup>a</sup>	8.58±0.11 <sup>a</sup>	8.73±0.19 <sup>a</sup>	8.69±0.1 <sup>a</sup>

The lowercase letters represent a significant difference between treatments (*P* < 0.05).

**Table 2.** The measured amounts (mean ± SE) of parameters in the inlet and outlet of the biological reactor during the experiment

Parameter	Wastewater inlet	Out let (First week)	Out let (Second week)	Out let (Third week)	Control treatment
NO <sub>3</sub> (mg L <sup>-1</sup> )	83.2	35.13±7.2 <sup>b</sup>	28.91±3.42 <sup>c</sup>	24.53±5.61 <sup>d</sup>	48.61±7.2 <sup>a</sup>
PO <sub>4</sub> (mg L <sup>-1</sup> )	14.7	6.48±0.44 <sup>b</sup>	4.92±0.11 <sup>c</sup>	4.34±0.39 <sup>c</sup>	8.52±1.27 <sup>a</sup>
DO (mg L <sup>-1</sup> )	1.27	4.31±1.87 <sup>b</sup>	4.47±1.53 <sup>b</sup>	4.57±1.27 <sup>b</sup>	5.17±2.18 <sup>a</sup>
pH	7.58	8.53±0.19 <sup>a</sup>	8.46±0.23 <sup>a</sup>	8.57±0.26 <sup>a</sup>	8.69±0.1 <sup>a</sup>

The lowercase letters represent a significant difference between treatments (*P* < 0.05).

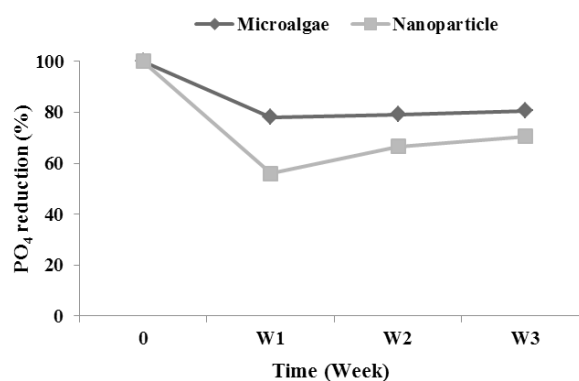
obtained results in the nanoparticle reactor, the amounts of nitrate compared with inlet wastewaters were decreased about 74.25, 77.64, and 80.76% whereas these amounts were decreased about 57.78, 65.26, and 70.52% in the biological reactor during three weeks (Figure 5). Also, the amounts of phosphate in the nanoparticle reactor were decreased about 78.17, 79.12, and 80.55% while the amounts of phosphate were decreased about 55.92, 66.54, and 70.48% in the biological reactor (Figure 6).

The particle size of iron oxide nanoparticles solution in the nanoparticle reactor space is shown in Figure 7. Accordingly, 95% of the particles in the suspension solution were 85 nm in diameter, indicating that particles were not deposited on the bottom of the reactor tank.

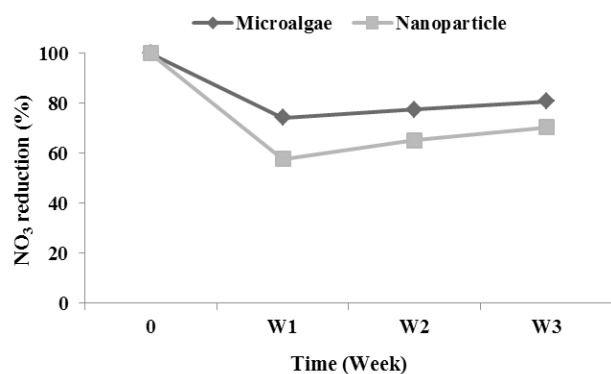
**Discussion**

Nowadays, the quantity of available freshwater has been decreased. Also, water sources have been contaminated by the industrial activities and urbane wastewaters (23,24). Pollution of water resources is one of the most important

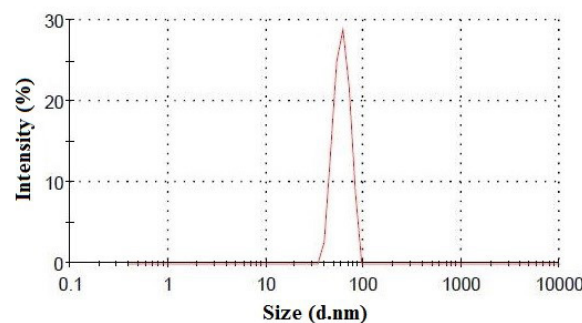
environmental problems in the world (25-27). Microalgae have the potential to eliminate inorganic nutrients such as phosphorus and nitrogen from wastewater, and hence, received significant consideration in the recent years (28). According to the results, the amounts of nitrate and phosphate were significantly decreased after three weeks



**Figure 6.** Comparison of the phosphate reduction using nanoparticle and biological reactors during the experiment.



**Figure 5.** Comparison of the nitrate reduction using nanoparticle and biological reactors during the experiment.



**Figure 7.** The particle size of iron oxide nanoparticles solution in the nanoparticle reactor.

in the biological reactor (Table 1 and Figure 5). Therefore, the use of *C. vulgaris* was desirable in this study, which is consistent with the results of other studies (23,29-31). The advantage of using algae in wastewater treatment systems is the recycling of food and its consumption by algae, which reduces the probability of eutrophication and other ecological damages (32). Voltolina et al used *Scenedesmus quadricauda* to test the removal of ammonia and found that microalgae such as *Scenedesmus* can be used in breeding systems as an appropriate option for wastewater treatment due to high growth, simple and cost-effective technology (29). Zhang et al observed that *S. quadricauda* and *C. vulgaris* removed about 100% nitrogen, phosphorus, and ammonia at the final purification stage (30). The efficiency of algae in wastewater treatment depends on the type of species, algal mass volume, pH, aeration, and time to maximize the activity of algae in the wastewater (13,15). Tang et al investigated the reduction of nitrogen and phosphorus in effluents using spirulina and found that it needs phosphorus and nitrate in the culturing process and culturing of spirulina in wastewater could decrease nitrate content from  $16 \pm 4.30$  to  $5.5 \pm 1.50$  ppm (31). According to a study by Sayadi et al, the amounts of nitrate and phosphate removal by *C. vulgaris* and *S. platensis* were significant, therefore, these microalgae can be effectively used to remove nitrate and phosphate from wastewaters (23). In another study by Sabeti et al on the enhanced removal of nitrate and phosphate from wastewater by *C. vulgaris* (temperature =  $26.3^{\circ}\text{C}$ , pH = 8, and aeration rate =  $4.7 \text{ L min}^{-1}$ ), approximately 85% of the total nitrate and 77% of the total phosphate were removed after 48 and 24 hours, respectively (33). During the experiment, the reduction percentages of nitrate and phosphate were acceptable in the nanoparticle reactor, but the values were lower compared to those obtained from the biological reactor (Figures 5 and 6). Iron oxide nanoparticles with low harmfulness, chemical inertness, and biocompatibility show a significant potential in combination with biotechnology (34). The removal of nitrate using zero-valent iron nanoparticles is very desirable due to the simplicity of the system, rapid reaction, low cost, and high removal efficiency from the engineering and economic point of view (10). Chen et al examined the removal of nitrate by a fluid substrate containing iron nanoparticles and observed that the removal of nitrate ion under optimum conditions was 85% (35). Malakootian et al reported that the Fenton process with zero-valent nanoparticles could be effective in reducing nitrate under optimum conditions during the process of absorbing  $\text{Fe}/\text{H}_2\text{O}_2$  in the removal of nitrate from water and could be used to remove similar compounds (36). The use of iron compounds at low pH levels in the presence of hydrogen peroxide can have a beneficial effect on the nitrate decomposition. This process can be used for the chemical reduction of nitrate in the contaminated groundwater (16). The study of Rafati et al on the removal

of phosphate by iron nanoparticle resin, Lewatit (FO36), showed that the concentration of phosphate reached  $1.6 \text{ mg g}^{-1}$  while the initial concentration of phosphate was  $6 \text{ mg L}^{-1}$  (37). Bani Najjar showed that zero-valent iron can be used to remove nitrate due to its unique regenerative property, surface area, and high activity as a coating on the carbon substrate (38). Cao et al reported that the removal efficiency of phosphate using iron oxide nanoparticles synthesized by eucalyptus leaf extract in the presence of cetyltrimethylammonium bromide surfactant increased from 71.0% to 97.3% (39). Based on a study by Khodadadi et al. (2017), the powdered activated carbon sorbent coated with magnetic iron nanoparticles has a desirable capability in the removal of phosphate from aqueous environments (40).

### Conclusion

Unrefined sewage can result in many environmental problems. The use of systems with low energy consumption will reduce the wastewater treatment, which can be appropriate for environmental management. According to the results, nitrate and phosphate levels in both reactors were significantly reduced compared to the control treatment. Also, the biological reactor was more effective in removing nitrate and phosphate than the nanoparticle reactor. Therefore, in order to increase the efficiency of wastewater removal, a simultaneous system of algae films and nanoparticles can be useful.

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### Ethical issues

The authors have thoroughly observed ethical issues and certify that no data from the study has been or will be published separately elsewhere.

### Competing interests

The authors declared no competing interests.

### Authors' contributions

All authors contributed in all aspects of this research like performing surveys and experiments, preparing the figures and tables, designing the experiments, analyzing the graphical data, writing the manuscript, and providing a critical revision of the paper.

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