

The removal of color and COD from wastewater containing water base color by coagulation process

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ABSTRACT: In this study acrylic water base color was removed from synthetic wastewater using coagulation process. Experiments were conducted on the sample containing 100 mg/L and 400 mg/L of acrylic water base color. Destruction of color by means of coagulation/flocculation techniques using ferrous sulfate, alum, lime and polyelectrolyte (cationic, anionic and non ionic). The study was performed in a systematic approach searching optimum values of alum and FeSO_4 concentration, pH and temperature. All the experiments were run in a laboratory scale. The obtained results show that treatment with alum and ferrous sulfate alone proved to be very effective in removing the color (> 99 %) and part of COD (60-70 %) from aqueous solution. Lime alone did not significant change on COD and color removal.

Key words: Color and COD removal, coagulation, ferrous sulfate, alum, lime, aqueous solution

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INTRODUCTION

Water base paint were the earliest type of paint and go to the dawn of history. Water born coating have been around in one form or another for decades but have demonstrated greatly improved performance characteristics in recent years. Water base or aqueous coating can be divided roughly in to three types. Water-soluble or water-reducible coating are coatings in which a resin is actually dissolved in the water phase. Colloidal or water solubilized dispersion coating are on intermediate between water soluble and emulsion coatings. Latex or emulsion coatings have resins dispersed in water that are stabilized by emulsifiers rather than dissolved. Acrylic paint is a synthetic media made by suspending pigment in synthetic polymer emulsified by water. They are essentially plastic paints that are water soluble and have good adhesive qualities. They are very stable and resist oxidation and chemical decomposition and will not yellow over time. The release of colored wastewater in the environment is considerable source of non aesthetic pollution and eutrophication and can originate dangerous by products through oxidation; hydrolysis or other chemical reaction taking place in the wastewater phased colorization of dye effluents

has therefore received increasing attention. For removal of color pollutants, adsorption on activated carbon, ultrafiltration, reverse osmosis, coagulation by chemical agent, ion exchange on synthetic adsorbent resins, ozonation and advanced oxidation processes (O_3/UV , $\text{H}_2\text{O}_2/\text{UV}$, $\text{O}_3/\text{H}_2\text{O}_2/\text{UV}$, $\text{Fe}^{2+}/\text{H}_2\text{O}_2$) can be used. (Azbar *et al.*, 2004 and Kusvuran *et al.*, 2004).

MATERIAL AND METHODS

Coagulation and flocculation

Experimental study was designed to obtain maximum COD and color removal at optimum pH temperature and FeSO_4 and alum doses. Aluminum sulfate ($\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$) and ferrous sulfate ($\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$) of commercial grade were utilized for the experimental procedure. A series of jar test experiment after adding coagulants applying 2 min rapid mixing at 120 rpm, 20 min slow mixing at 30 rpm and 45 min settling was conducted by using 500 mL dye solution. (Georgiou, *et al.*, 2003).

Analytical methods

COD was measured according to standard methods. Absorbance measurements were made using pu 8700 series uv/vis spectrophotometer for color removal. The

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supernatant in each beaker were filtered by 0.45 μm millipore membrane filter before measuring COD and absorbance at maximum wave length. Removal efficiency of COD and color were obtained according to the formula given below. (Georgiou, *et al.*, 2003).

$$\text{Removal (\%)} = (c/c_0) / c_0$$

Where c_0 and c are the initial and final absorbance or COD values of simulated wastewater, respectively.

RESULTS

Coagulation with ferrous sulfate

Basic equations occurring during the coagulation process for ferrous sulfate is given with equation 1:

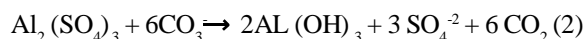


Varying ferrous sulfate concentration (1000 mg/L) keeping pH constant (9) were applied for the treatment of wastewater. A ferrous sulfate concentration of 200 mg/L and 100 mg/L was necessary for an efficient COD

removal for 400 and 100 mg/L color concentration and did not significant change COD removal.

Coagulation with aluminum sulfate

Aluminium ion, Al^{+3} , behaves very much like Fe^{+3} . When alum is added to water or wastewater $\text{Al}(\text{OH})_3$ precipitations occurs as described by the following equation 2:



Similar to ferrous sulfate experiment, varying aluminum sulfate concentration, keeping pH at the optimum condition 10 were applied for the treatment of wastewater. An alum concentration of 600 mg/L and 300 mg/L was necessary for an efficient COD removal for 400 and 100 mg/L color concentration. $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$ and $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ coagulant were used during the chemical treatment experiments with varying dosages under varying pH condition. For comparison the COD and color removal results of under best pH condition are given in Figs. 1-4 and Table 1.

Table 1: Optimum removal condition for WBA using coagulation process

WBA Color (mg/L)		100	400
COD removal (%)	Alum	69	70
	Ferrous sulfate	67	69
COLOR removal (%)	Alum	99.8	99.99
	Ferrous sulfate	98.7	99.6
pH	Alum	10	10
	Ferrous sulfate	9	9
T ($^{\circ}\text{C}$)	Alum	40	40
	Ferrous sulfate	30	30
Concentration (mg/l)	$\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$	100	200
	$\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$	300	600

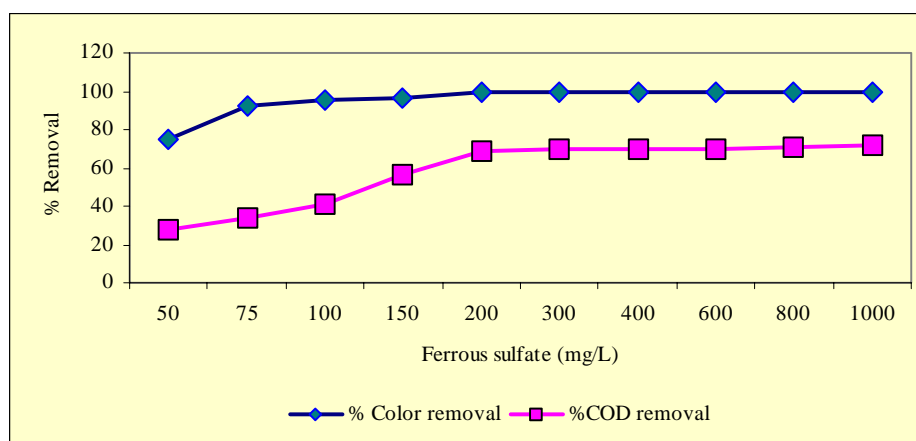


Fig.1: Effect of FeSO_4 concentration on COD and color removal (400 mg/L WBA) at 9.0 pH

The removal of color...

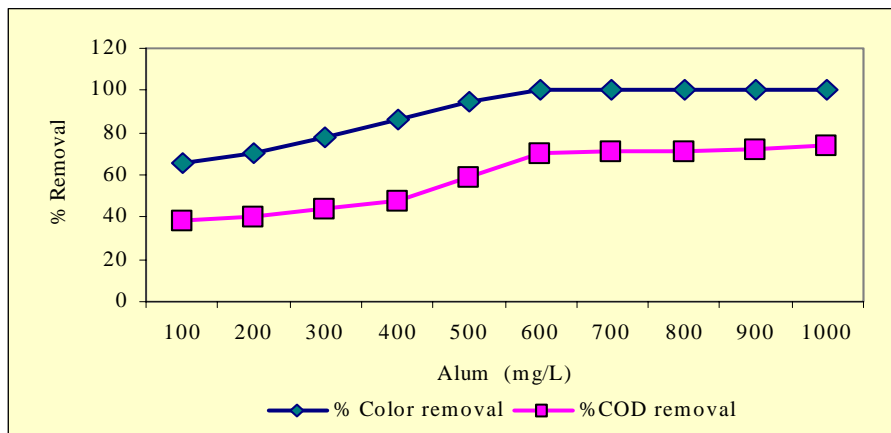


Fig. 2: Effect of Alum concentration on COD and color removal (100 mg/L WBA) at 10.0 pH

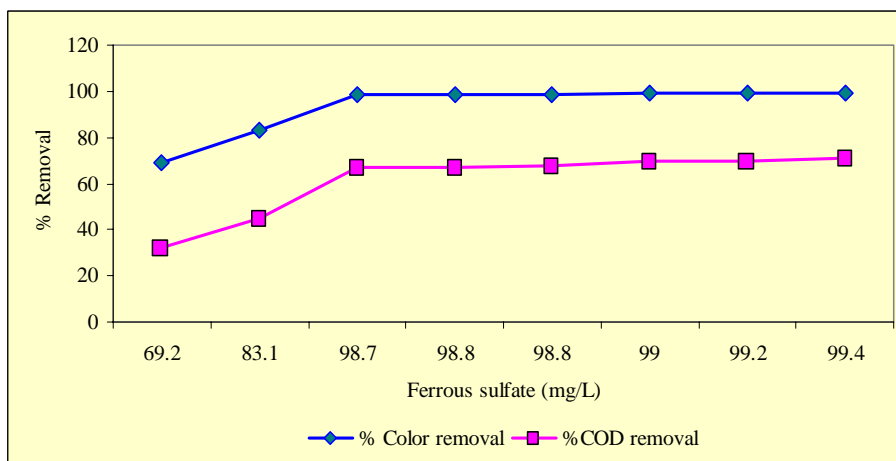


Fig. 3: Effect of FeSO_4 concentration on COD and color removal (100 mg/L) at 9.0 pH

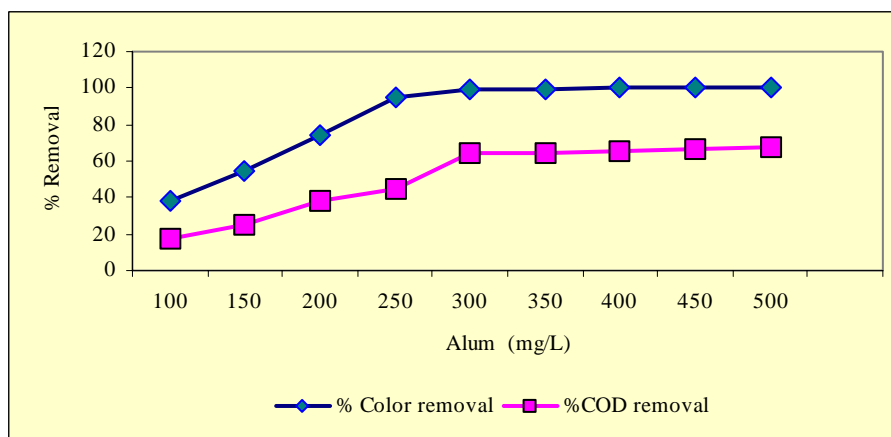


Fig. 4: Effect of Alum concentration on COD and color removal (100mg/l WBA) at 10.0 pH

Optimum pH and temperature for each coagulant was found to be as follow: pH=3, T=40 for alum and pH= 9, T= 30 for $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$. In term of COD removal, alum and ferrous sulfate used behaved same from the practical point of view as follow: 70 % COD (COD in effluent = 120 mg/L) and 99.99 % color removal were observed in experiments using $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$ with a dose of 600 mg/L For 400 mg/L of WBA, and for 100 mg/L WBA 69 % COD (COD in effluent = 124 mg/L) and color removal by $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$ with a dose of 300 mg/L was 99.8 %. While the COD removal at a FeSO_4 dose of 200 mg/L resulted in an effluent COD of 124 mg/L (69% COD removal) for 400 mg/L WBA and by 100 mg/L FeSO_4 for 100 mg/L WBA 67% COD removal (COD in effluent = 132 mg/L) were observed. Color removal by lime with a dose of 2000 mg/L and 1000 mg/L was 37 % and 15 % for 400 and 100 mg/L color concentration, respectively. COD removal by lime was very low. By using 10 mg/L polyelectrolyte (cationic, anionic and non ionic) with alum and ferrous sulfate did not significant change on flocculation and size of floces.

DISCUSSION AND CONCLUSION

Degradation of acrylic water base color in aqueous solutions by the coagulation process was performed. Color removal by coagulation process by use of alum and ferrous sulfate was > 99 % and COD removal is approximately 70 %. But lime was not effective on color and COD removal and polyelectrolyte did not significant change on flocculation. Before treatment wastewater by alum and ferrous sulfate pH must be adjusted and so alkanity was necessary to coagulation that must be adjusted by lime or calcium carbonate, but in this study alkanity of sample was enough. But due to the high chemical sludge production and increasing of hardness and corrosion it seems coagulation was not applicable for color removal in the wastewater containing color.

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