

Decolorisation of exhausted reactive dye bath using ozonator for reuse

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ABSTRACT: Exhausted Reactive dye bath samples of Turquoise Blue, Olive Green and Navy Blue shades were collected from cotton knit wear dyeing units in Tirupur. Ozonation was conducted in a column reactor system fed with ozone at the rate of 0.16 g/min to assess its efficiency in reducing the color, chemical oxygen demand and total organic carbon. Complete decolorization of the effluent was achieved in 10 min contact time and ozone consumption of 153 mg/L for Turquoise Blue, 128 for Olive Green and 143 for Navy Blue shades effluents respectively. The corresponding COD removal was 43 %, 44 % and 43 % for the three shades while TOC removal efficiency was 45 %, 45 % and 40% respectively. The results from the reusability studies indicate that the dyeing quality was not affected by the reuse of decolorized dye bath for two successive cycles. It is concluded that ozonation is efficient in decolorization of exhausted dye bath effluents containing conventional reactive dyes. However, the corresponding removal of COD from the textile effluent was not significant.

Key words: Gas turbine, reheat, recuperator, advanced cycles

INTRODUCTION

Textile industry is one of the most complex industries among the manufacturing industries. Various textile chemicals such as wetting agents, dyes, surfactants, fixing agents, softeners and many other additives are used in wet processes such as bleaching, dyeing and finishing processes. As a result, textile wet processing plants produce highly polluting wastewater (Ademorotti, 1992; Navarro, 2001; Wang, 2002; Sheng and Chi, 1993). Textile dyeing effluents are intensely colored and known to present extreme variations of pH and temperature, high COD and Dissolved Solids (Sevimli and Kinaci, 2002; Sheng and Chen, 1997; Sevimli and Sarikaya, 2002). Strong color of the textile wastewater is the most serious problem of the textile waste effluent. Treatment of wastewater containing reactive dyes is a severe problem for the cotton textile industry (Frank, 1994). Ozonation is perhaps the most advanced method ever attempted for decolourisation of the textile effluents (Snider and Porter, 1994; Beszedits, 1980; Green and Sokol, 1985; Gould and Groff, 1987). It is well known that ozone is a powerful oxidant and its oxidizing potential is nearly twice that of chlorine. The high oxidation potential allows ozone to degrade most organic compounds (Chu and Ma, 2000). Ozone and hydroxyl radical (HO°) species

generated in aqueous solution are able to open aromatic rings. Ozone alone and in combination with UV light, catalyst, ultrasound or activated carbon has been successfully applied to textile industrial effluents (Maggiolo, 2000). The advantage is that ozone can be applied directly in its gaseous state and therefore doesn't increase the volume of wastewater and sludge (Sheng and Chi, 1993). This paper presents the results of the studies on decolorization of medium shade dye bath wastewaters originating from cotton knit wears textile industry by ozonation for potential reuse.

MATERIALS AND METHODS

The overall schematic of the methodology followed is presented in Fig. 1.

The exhausted dye bath samples of Turquoise Blue, Olive Green and Navy Blue shades were collected from Tirupur textile dyeing industries. The samples were characterized, decolorized by ozonation and reused for dyeing. The studies were repeated in 3 cycles. In all the samples were analyzed for pH, Color, COD and TOC based on Standard Methods (APHA, 1998).

Ozonation studies were done using an experimental set up consisting of ozonator, oxygen concentrator and bubble column reactor and air diffuser as depicted in Fig. 2. Ozone was generated from concentrated oxygen by Indizone Model Ozone generator. The production capacity of ozone generator is 10g/h. A cylindrical

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Borosil glass reactor of 10 cm diameter and 200 cm height was used for the ozonation. Silicon tubing was used for the connection between oxygen concentrator and ozone generator. Ozonator to column reactor acrylic tube was used. A tubular cylindrical porous diffuser was connected to the acrylic tube and placed at the bottom of the reactor to transfer ozone gas into aqueous solution. Two reactors containing 2 L of 2% KI solution was used to trap the ozone in off gas. Sodium thiosulphate titration procedure (APHA, 1998) was performed to measure the ozone concentration, trapped in the KI solutions from which the ozone dose required for complete decolorization of dye bath was determined. All experiments were performed at ambient temperature (28-30°C). 10 L of the exhausted reactive dye bath (Turquoise Blue, Olive Green, Navy Blue) samples were subjected to ozonation for 10 min contact time at an ozone dose of 0.16 g/min. The samples that were decolorized during this period were turbid. These were subjected to filtration using 5 micron filter at an operating pressure of 1.0 bar.

The exhausted dye bath and decolorized, samples were analyzed for pH, color, COD and total organic carbon (TOC) based on Standard Methods (APHA,

1998). Total organic carbon (TOC) of the exhausted dye bath and decolorized dye bath were measured using a TOC analyzer (Micro N/C Model 1997, Analytica Jena, Germany). COD was measured according to Standard Methods (APHA, 1998). Colour of the samples was determined by absorbance measurements using Spekol 1200 model spectrophotometer at three different wavelengths (436, 525 and 620 nm) based on German method (Frank, 1994). The dye bath samples after decolorization (10 min ozonation + filtration) were used for dyeing 10 g sample of bleached and fluorescent brightener free knitted cotton fabric in a laboratory dyeing machine. The dyes used in this study, their colour Index generic name, λ_{max} , chemical constitution and type are provided in Table 1. The recipe for the dyeing studies and quantity of dyes for the dyeing of 10 g knitted cotton fabric is given in Table 2. The dyeing studies were also repeated using tap water and salt for comparison of dyeing quality. A Laboratory dyeing machine with 12 numbers of 250 mL stainless steel tumblers was used for dyeing. The tumblers were filled with 200 mL of decolorized dye bath or tap water and heated to 40 °C. The dyestuff and exhausting agent (NaCl) were added in the case of tap water (based on

Table 1: Properties of the dyes used in dyeing studies

Sl. No.	CI Name	λ_{max} (nm)	Chemical constitution	Type
1	CI Reactive Red 120	510	Diazo, Dichlorotriazine	Salt controllable high substantivity
2	CI Reactive Yellow 84	420	Diazo, Bisaminochlorotriazine	Salt controllable high substantivity
3	CI Reactive Blue 5	620	Diazo, Bis (sulphatoethylsulphonate)	Alkali controllable low substantivity

Table 2: Recipe for reactive dyeing

Sl.No.	Parameter	Values
1	Shade	Turquoise Blue, Olive Green , Navy Blue
2	Weight of Knitted fabric (g)	10
3	Material Liquor ratio	1:20
4	% of Shade	2.0 %
5	Dye (mg)	0.2
6	Dyeing time (min)	90
7	NaCl (g/L)	60*
8	Na ₂ CO ₃ (g/L)	15
9	Temperature (°C)	70-80

* Only for tap water

the dyeing recipe) while only dyestuff was added for the decolorized dye bath.

Fabric was wetted and immersed in the dye bath and dyeing was done as temperature gradually increased from 40 °C to 60 °C in 30 min. At this temperature, alkali (Na₂CO₃) was added and dyeing was continued at 80°C for 60 mins. After dyeing, the fabric was removed from the dye bath and hot wash (90 °C for 10 min) was done twice. Then the fabric was neutralized using 0.1 g/L glacial acetic acid at 27-30 °C for 10 min. Soaping with 2 g/L soap solution at 90°C for 10 min was done followed by two cold washes at 27-30 °C for 10 min after which the dyed fabric was air dried.

The dyed fabric was tested for colour strength using UV-Visible Spectrophotometer U-3210 (Make: Hitachi).

The K/S value as per Kubelka - Munk equation has a linear relationship with the concentration of colorant and is calculated using Eq,

$$K/S = \frac{(1-R)^2}{2R}; \text{ where R is the reflectance (\%)}$$

Wash fastness of dyed sample was measured using ISO Test 3 (ISO 105-C03: 1989, Geneva) testing method. Dyed fabric sample (10cm x 4 cm) was taken, stitched with one of the shorter side of the adjacent bleached fabric and put into the water bath at 60°C for 30 min.. Then the specimen was washed with hot water, cold water and dried.

After dyeing (cycle-I), the exhausted dye bath samples from laboratory dyeing were analyzed for pH, color, COD and TOC and subjected to ozonation for 10 min and micron filtration. The decolorized samples were used for dyeing (cycle II) and the procedure repeated once again (cycle III).

RESULTS

The results of the decolorisation studies are presented in Table 3. The color of Turquoise Blue shade dye bath was reduced by 58%, 67% and 55% at 436 nm, 525nm and 620 nm respectively at an ozone contact time of 10 minutes. The ozone consumption during the period was 153 mg/L. Micron filtration of this sample improved the over all color removal to 74, 75 and 92 % at the three wavelengths. The color of Olive Green was reduced by 98%, 63% and 74% at 436nm, 525 nm and 620 nm respectively at an ozone contact time of 10 minutes. The ozone consumption during the period was 128 mg/L. Micron filtration of this sample improved the over all colour removal to 99%, 78% and 83 % at the three wavelengths respectively. The color of Navy

Blue was reduced by 100%, 93% and 90% at 436nm, 525 nm and 620 nm respectively at an ozone contact time of 10 minutes (Fig. 5). The ozone consumption during the period was 142.5 mg/L. Micron filtration of this sample improved the over all colour removal to 100, 94 and 90 % at the three wavelengths respectively.

The results of the COD and TOC removal by ozonation is presented in Fig. 3. It was observed that the COD removal for Turquoise dye bath was 29 % while TOC removal was 32%. Micron filtration improved it to 43 % for COD and 45 % for TOC removal. It was observed that the COD removal (31 %) and TOC removal (31%) for Olive Green dye bath was low at a contact time of 10 minutes. Micron filtration improved it by 44 % for COD and 45 % for TOC removal. It was observed that the COD removal (27 %) and TOC removal (21%) for Navy Blue dye bath was low at a contact time of 10 minutes. Micron filtration improved it by 43 % for COD and 40 % for TOC removal. The results of the decolorisation studies are for cycle II and III are presented in Tables 4 and 5. For cycle II, decolorization of 57 %, 67% and 57 % was observed for Turquoise Blue shade dye bath, at 10 min contact time which increased to 71 %, 73 % and 71 % at 436, 525,620 nm respectively after micron filtration. A similar increase was observed for cycle III.

For Olive Green dye bath, at 10 min contact time decolorization of 98 %, 67% and 79% was observed which increased to 98 %, 74 % and 82 % at 436, 525,620 nm respectively after micron filtration for cycle II. A similar increase was observed for cycle III. For Navy Blue dye bath, at 10 min contact time decolorization of 100 %, 91 % and 90 % was observed which increased to 100 % at 436, 525,620 nm respectively after micron filtration for cycle II.

Table 3: Decolourisation (%) of reactive dyebaths by ozonation for Cycle 1

Time	Turquoise Blue			Olive Green			Navy Blue		
	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm
1	11	50	20	8	8	10	9	7	15
2	16	50	22	16	10	12	22	26	33
3	16	50	24	45	12	20	84	83	48
4	21	58	25	83	32	31	84	85	63
5	26	58	27	93	48	49	91	88	65
6	32	58	28	96	52	53	97	90	68
7	37	67	30	96	53	54	98	91	69
8	42	67	39	89	61	63	100	91	87
9	47	67	46	98	67	70	100	92	88
10	58	67	55	98	63	74	100	93	90
10 + F *	74	75	92	99	78	83	100	94	90

* Filtration

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Table 4: Decolourisation (%) of reactive dyebaths by ozonation for Cycle 2

Time	Turquoise Blue			Olive Green			Navy Blue		
	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm
1	5	13	19	2	6	11	6	3	15
2	10	47	23	9	10	20	15	23	33
3	14	53	39	14	12	33	65	81	48
4	19	60	43	38	19	42	71	84	63
5	24	60	43	69	24	47	79	87	65
6	29	67	43	94	33	59	86	90	68
7	43	67	43	95	51	64	90	90	69
8	48	67	43	94	55	69	95	91	87
9	52	67	51	97	59	74	96	91	88
10	57	67	57	98	67	79	100	91	90
10+									
F	71	73	77	98	74	82	100	100	100

Table 5: Decolourisation (%) of reactive dyebaths by ozonation for Cycle 3

Time	Turquoise Blue			Olive Green			Navy Blue		
	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm	436 nm	525 nm	620 nm
1	5	50	20	2	6	11	6	3	15
2	11	50	22	9	10	20	15	23	33
3	16	50	24	14	12	33	65	81	48
4	21	58	25	38	19	42	71	84	63
5	26	58	27	69	24	47	79	87	65
6	32	58	28	94	33	59	86	90	68
7	37	67	30	95	51	64	90	90	69
8	42	67	39	94	55	69	95	91	87
9	47	67	46	97	59	74	96	91	88
10	58	67	55	97	61	75	95	91	90
10+									
F	74	75	92	98	68	79	96	92	90

A similar increase was observed for cycle III.

From the results of COD and TOC removal resented in Figure 4 and 5, it is observed that for Olive Green dyebath, TOC and COD removal was 32 % in the second cycle, which further increased to 45% on microfiltration. For Olive green dyebath, the COD/TOC reduction was 30 %, which increased to 44 % on microfiltration. A similar observation for navy blue shade was also seen. A similar trend was seen for third cycle with the TOC/COD removal ranging between 25 % to 34 % and increasing to 42 % to 45 % after micron filtration. The K/S value and wash fastness of the fabric dyed with tap water and decolorized dye bath obtained in the the different cycles is presented in Table 6. The first cycle showed little variation with a difference of 0.0038 for Turquoise Blue, 0.0057 for Olive Green and 0.0027 for Navy Blue shade. A similar trend was observed for wash fastness, as the grey scale value of tap water when compared with the three shades did not show variation. When the K/S value of the fabric dyed with tap water and decolorized dye bath obtained from cycle II and III were compared, there was a significant deterioration of quality in cycle III. The difference was 0.0058 for cycle II and 0.0598 for cycle III for Turquoise Blue, 0.0077 for cycle II and 0.1625 for cycle III for Olive Green and 0.0053 and 0.0896 for cycle II and III for Navy Blue shade respectively. A similar trend was observed for wash fastness, as the grey scale value was lower for cycle III when compared with other shades/ cycles. Cycle II and I produced good wash fastness when compared to cycle III.

DISCUSSION AND CONCLUSION

These results are in line with the decolorisation efficiency of 95% (Balcioglu and Arslan, 2001), 71 % (Ramasamy et al., 2001) and 90 % at 5 min ozonation time (Assalin, et al., 2004) at ozone dose of 15 and 14g/L respectively. Complete color removal of dye bath at 60 min ozonation time has also been reported (Balcioglu and Arslan, 2001; Arslan, 2000) at an ozone dose of 35 mg/L. For Navy blue shade, micron filtration did not have any effect for increasing color removal while for Olive green and turquoise blue shades there was a significant increase in color removal after micron filtration. It was reported (Oguz et al., 2005) that though ozonation is an efficient process for dye removal, COD removal was rather inefficient, usually not exceeding 54 %. The reduction of COD and TOC for Turquoise Blue, Olive Green and Navy Blue shade dye bath was low and did not show much variation. Approximately a reduction of 40-45 % COD was achieved after 10 minutes of ozonation followed by micron filtration. This was comparable with the reported values for COD reduction of 11-29 % (Perkowski, et al., 2000), 50 % (Selcuk, 2005), 27-87 % (Wu and Wang, 2001) and 5-20 % (Frank, 1994) respectively. A TOC reduction of 5 % at 5 min contact time and 43 % at 60 min contact time was reported (Balcioglu and Arslan, 2001). In other studies, 50 % TOC removal (Ince and Tezcanli, 2001) and 48-62 % removal at 5 min contact time has been reported (Arslan and Balcioglu, 2000). The increase in COD and TOC in successive cycles could be attributed to increased residual by-products of ozonation with each cycle of reuse. The increase in TOC removal after

Table 6: K/S and wash fastness of dyed fabrics

Sl.No.	Reuse cycle	Shade	K/S	Wash fastness	
				Change in shade	Change in stain
1	Standard (Tap Water)	Turquoise	0.5563	4-5	4-5
		Blue			
		Olive	0.7754	5	5
		Green			
2	Cycle 1	Navy	0.7911	5	5
		Blue			
		Turquoise	0.5525	4	4
		Blue			
3	Cycle 2	Olive	0.7703	5	5
		Green			
		Navy	0.7884	5	5
		Blue			
4	Cycle 3	Turquoise	0.5505	3-4	3-4
		Blue			
		Olive	0.7677	4	4
		Green			
4	Cycle 3	Navy	0.7858	4	4
		Blue			
		Turquoise	0.4965	2-3	2-3
		Blue			
4	Cycle 3	Olive	0.6129	3	3
		Green			
		Navy	0.7015	3	3
		Blue			

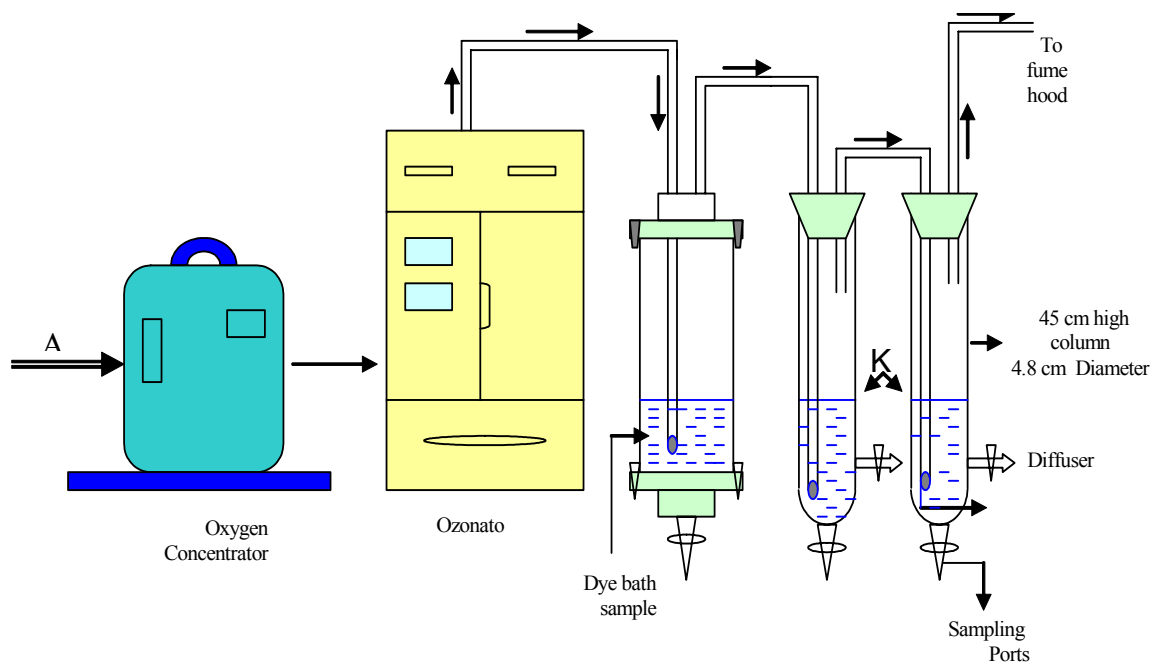


Fig. 1: Experimental setup for ozonation

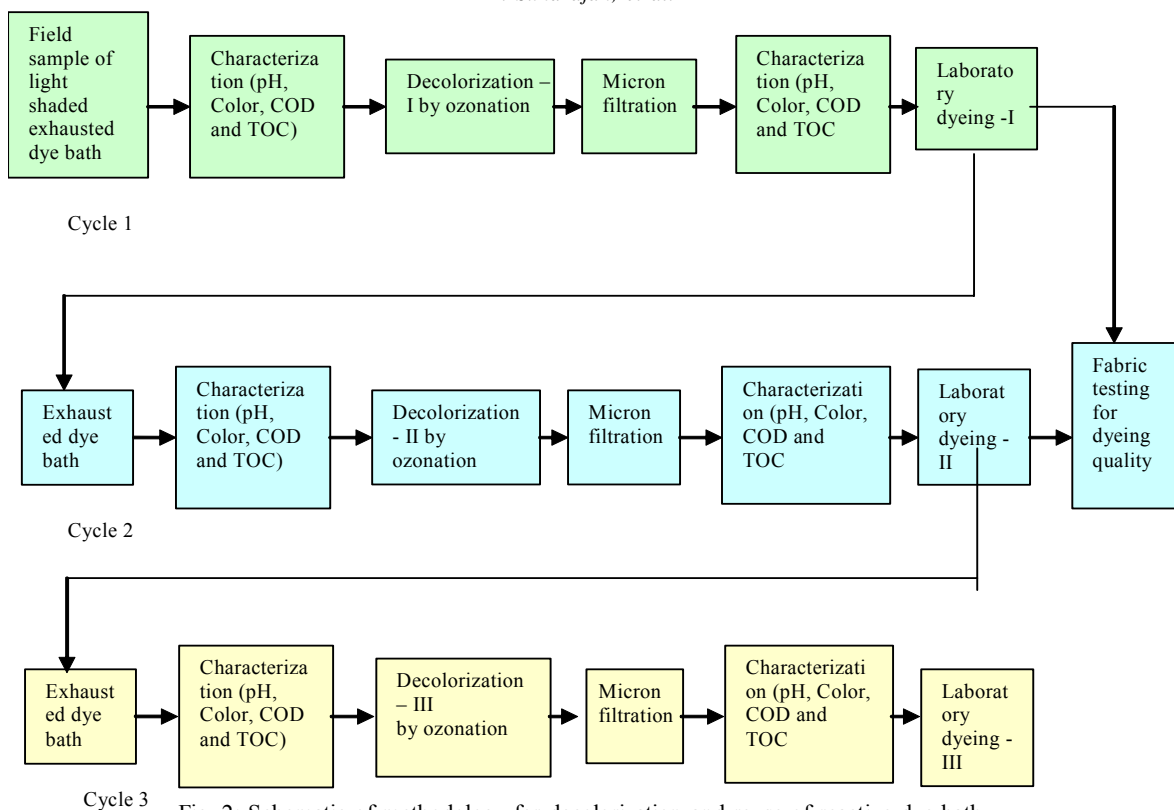


Fig. 2: Schematic of methodology for decolorization and reuse of reactive dye bath

micron filtration is from the reason that the organic particulate matter causing turbidity and contributing to the TOC/COD of the effluent is removed. Significantly the high COD and TOC of the decolorized dye bath obtained in the first cycle I did not affect the quality of the subsequent dyeing, while the increase of COD and TOC in the cycle II affected the quality of the third cycle. The results of the present studies show that ozonation is effective in complete decolorisation of exhausted dye bath effluent. The associated COD and TOC reduction was low. At a contact time of 10 minutes and ozone consumption of 153 mg/L for Turquoise Blue, 128 mg/L for Olive Green and 143 mg/L for Navy Blue, 78 -100 % of color removal was achieved. Micron filtration played an important role in removing the turbidity that interfered with color measurement. The average COD removal, for the Turquoise blue, Olive Green and Navy Blue shades of exhausted reactive dye bath was 44 % while TOC removal was in the range of 40-45 %. This was similar to the COD removal efficiency for light shades achieved at less ozonation time. This implies that ozonation alone, is not a satisfactory method for removal of COD and TOC. Though the color is removed effectively, the by- products are still present in the decolorized dye

bath and contribute to COD and TOC. As micron filtration improved the TOC removal of the ozonated effluent it can be included as a posttreatment step after ozonation.

The results from the reusability studies of decolorized dye bath indicate that the dyeing quality was not affected for two successive cycles. The increase in residual COD and TOC affected the dyeing quality in the third cycle implying that ozonation was feasible for decolorisation of medium shaded dye bath for two cycles of reuse. This is in line with the results obtained from decolorisation and reuse of light shade dye bath. Further TOC/COD reduction is needed for its repeated reuse in more than two dyeing cycles.

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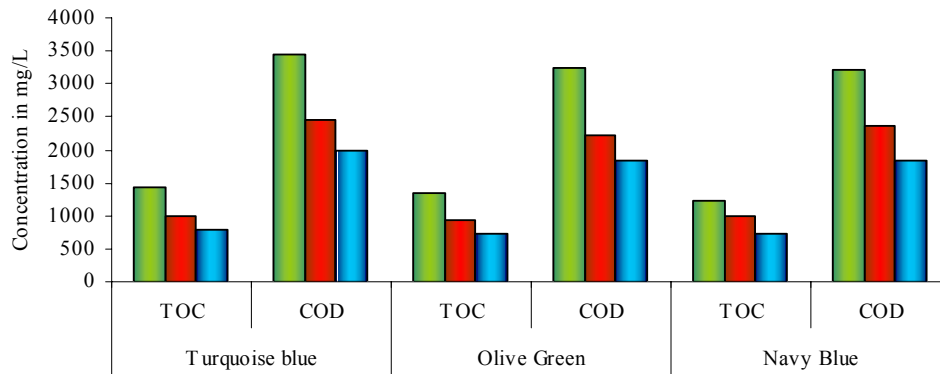


Fig. 3: COD and TOC removal by ozonation for Cycle I

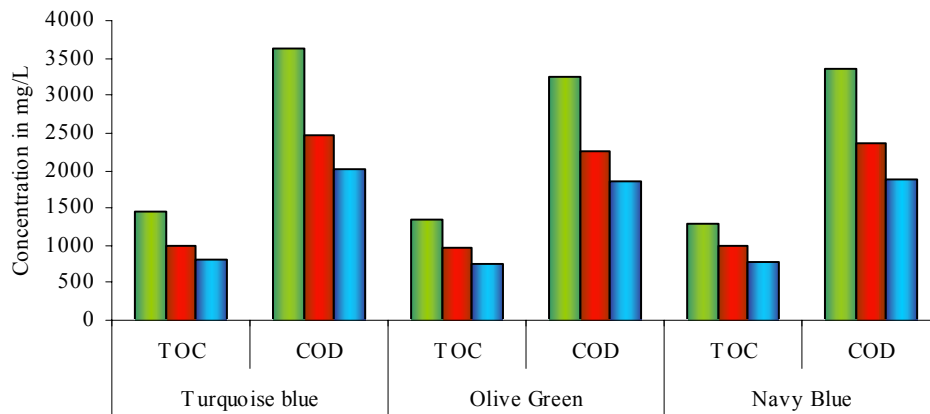
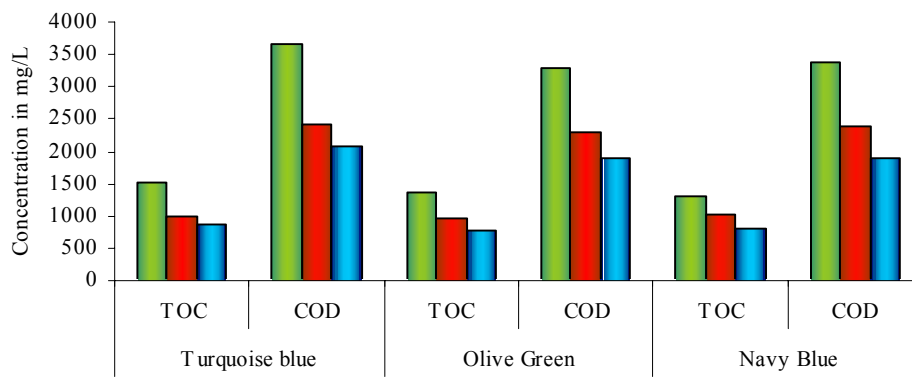


Fig. 4: COD and TOC removal by ozonation for Cycle II



■ Exhausted dyebath ■ Decolorised dyebath ■ Dyebath after micron filtration

Fig. 5: COD and TOC removal by

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