

# Research note MHD flow of a Casson fluid over an exponentially shrinking sheet

## S. Nadeem<sup>a</sup>, Rizwan Ul Haq<sup>a,\*</sup>, C. Lee<sup>b</sup>

<sup>a</sup> Department of Mathematics, Quaid-i-Azam University 45320, Islamabad 44000, Pakistan <sup>b</sup> Department of Computational Science and Engineering, Yonsei University, South Korea

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#### **KEYWORDS**

MHD; Casson fluid; Exponentially shrinking sheet; Adomian decomposition method; Padé approximation. **Abstract** The magnetohydrodynamic (MHD) boundary layer flow of a Casson fluid over an exponentially permeable shrinking sheet has been investigated. The analytical solution arising differential system has been computed by the Adomian Decomposition Method (ADM). Variations of interesting parameters on the velocity are observed by plotting graphs.

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#### 1. Introduction

The boundary layer flow over a shrinking surface is encountered in several technological processes. Such situations occur in polymer processing, manufacturing of glass sheets. paper production, in textile industries and many others. Crane [1] initiated a study on the boundary layer flow of a viscous fluid towards a linear stretching sheet. An exact similarity solution for the dimensionless differential system was obtained. Carragher and Carane [2] discussed heat transfer on a continuous stretching sheet. Afterwards, many investigations were made to examine flow over a stretching/shrinking sheet under different aspects of MHD, suction/injection, heat and mass transfer etc. [3-10]. In these attempts, the boundary layer flow, due to stretching/shrinking, has been analyzed. Magyari and Keller [11] provided both analytical and numerical solutions for boundary layer flow over an exponentially stretching surface with an exponential temperature distribution. The combined effects of viscous dissipation and mixed convection on the flow of a viscous fluid over an exponentially stretching sheet were

\* Corresponding author.

E-mail address: ideal\_riz@hotmail.com (R. Ul Haq).

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analyzed by Partha et al. [12]. Elbashbeshy [13] numerically studied flow and heat transfer over an exponentially stretching surface with wall mass suction. Sajid and Hayat [14] provided an analytical solution for boundary layer flow of a Jeffrey fluid over an exponentially stretching sheet. The numerical solution of the same problem was then given by Bidin and Nazar [15]. The effects of radiation on the MHD boundary layer flow of a viscous fluid over an exponentially stretching sheet were studied by Ishak [16].

To the best of our knowledge, no information is yet available for boundary layer flow induced by an exponentially shrinking sheet. The present work deals with the MHD flow of Casson fluid [17,18] induced by an exponentially shrinking sheet. The Adomian Decomposition Method (ADM) has been employed to obtain the analytical solution. This method has been successfully applied to various interesting problems [19–25]. The Padé approximation [26] is used to handle the boundary condition at infinity and to find the better convergence.

#### 2. Mathematical model

Let us consider the two-dimensional flow of an incompressible Casson fluid over an exponentially shrinking sheet. The fluid is electrically conducting in the presence of a uniform magnetic field applied normal to the sheet, and the induced magnetic field is neglected under the approximation of small Reynolds number. We also assume the rheological equation of

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Casson fluid, reported by Mustafa et al. [19], is:

$$\tau^{1/n} = \tau_o^{1/n} + \mu \dot{\gamma}^{1/n}.$$
 (1)

Or:

$$\tau_{ij} = \left[\mu_B + \left(\frac{P_y}{\sqrt{2\pi}}\right)^{1/n}\right]^n 2e_{ij},\tag{2}$$

where  $\mu$  is the dynamic viscosity,  $\mu_B$  is plastic dynamic viscosity of the non-Newtonian fluid,  $P_v$  is the yield stress of fluid,  $\pi$ is the product of the component of deformation rate with itself, namely,  $\pi = e_{ij}e_{ij}$ , and  $e_{ij}$  is the (i, j)th component of the deformation rate. An anonymous referee has suggested considering the value of n = 1. However, in many application this value is  $n \gg 1$ .

The problem is governed by the following equations:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{3}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = v\left(1 + \frac{1}{\gamma}\right)\frac{\partial^2 u}{\partial y^2} - \frac{\sigma B^2}{\rho}u.$$
 (4)

The boundary conditions are defined as:

$$u = U_w(x) = -U_0 \exp\left(\frac{x}{l}\right) \text{ and } v = V_w(x) = V_0 \exp\left(\frac{x}{2l}\right) \text{ at } y = 0,$$
  
$$u = 0 \quad \text{as} \quad y \to \infty.$$
(5)

In the above expression  $U_w$  is shrinking velocity with  $U_0$ (shrinking constant),  $V_w$  is mass transfer velocity with ( $V_0 > 0$ for mass injection and  $V_0 < 0$  for mass suction), u and v are components of velocity in x and y-directions, respectively, and l is the characteristic length. It is assumed that the magnetic field B(x) is of the form

$$B = B_0 \exp(\frac{x}{l})$$

where  $B_0$  is the constant magnetic field. We introduce stream function  $\Psi$  as:

$$u = \frac{\partial \Psi}{\partial y}$$
 and  $v = -\frac{\partial \Psi}{\partial x}$ , (6)

and define variables:

$$\Psi = \sqrt{2\nu l U_0} x f(\eta) \exp\left(\frac{x}{2l}\right),$$
  
and  $\eta = y \sqrt{\frac{U_0}{2\nu l}} \exp\left(\frac{x}{2l}\right).$  (7)

"With the help of the above transformation", equation of continuity (1) is identically satisfied and momentum Eq. (2) takes the form:

$$\left(1+\frac{1}{\gamma}\right)f'''-M^2f'+ff''-2(f')^2=0.$$
(8)

The corresponding boundary conditions are:

$$f = s, \quad f' = -1 \quad \text{at } \eta = 0,$$
 (9)

$$f' \to 0 \quad \text{as } \eta \to \infty,$$
 (10)

where  $M^2 = \frac{2\sigma B^2 l}{\rho U_0}$  is Hartmann number, and  $\gamma$  is Casson fluid parameter.

#### 3. Solution by Adomian Decomposition Method (ADM)

To solve the above dimensionless equation with given boundary conditions from Eqs. (6) to (8) with the help of ADM, we first write Eq. (6) in operator form as:

$$f''' = \left(\frac{\gamma}{1+\gamma}\right) (M^2 f' + 2f'^2 - f f''), \tag{11}$$

$$Lf = \left(\frac{\gamma}{1+\gamma}\right) (M^2 f' + 2f'^2 - ff''), \qquad (12)$$

where  $L = \frac{d^3}{dn^3}$ . Applying the inverse operator is defined as:

$$L^{-1}(*) = \int_0^{\eta} \int_0^{\eta} \int_0^{\eta} (*) dt dt dt.$$
(13)

Applying  $L^{-1''}$  on both sides of Eq. (12), we obtain:

$$L^{-1}(Lf) = f = \left(\frac{\gamma}{1+\gamma}\right) L^{-1}(M^2f' + 2f'^2 - ff''),$$
(14)

or:

1

$$= \left(\frac{\gamma}{1+\gamma}\right) \int_{0}^{\eta} \int_{0}^{\eta} \int_{0}^{\eta} (M^{2}f' + 2f'^{2} - ff'') dt dt dt.$$
(15)

With the help of boundary conditions (9) and (11), we can write Eq. (13) as:

$$f = s - \eta + \frac{\alpha}{2} \eta^{2} + \left(\frac{\gamma}{1 + \gamma}\right) \{(M^{2})L^{-1}(f') + 2L^{-1}(f'^{2}) - L^{-1}(ff'')\}, \quad (16)$$

where  $\alpha = f''(0)$  is to be determined, s is suction/injection at the wall. In ADM, the nonlinear terms in Eq. (16) can be decomposed as:

$$f'^{2} = \sum_{k=0}^{\infty} A_{k}, \qquad f f'' = \sum_{k=0}^{\infty} B_{k}.$$
 (17)

Adopting the algorithm for the Adomian polynomials proposed by Adomian [23], we defined:

$$A_{i} = \sum_{k=0}^{i} f_{k}' f_{i-k}' \qquad B_{i} = \sum_{k=0}^{i} f_{k} f_{i-k}'' \quad \forall i = 0 \cdots n.$$
(18)

Substituting Eq. (17) into Eq. (16) yields:

$$f = s - \eta + \frac{\alpha}{2}\eta^{2} + \left(\frac{\gamma}{1+\gamma}\right) \times \left\{ (M^{2})L^{-1}(f') + 2L^{-1}\sum_{k=0}^{\infty}A_{k} - L^{-1}\sum_{k=0}^{\infty}B_{k} \right\}.$$
 (19)

Hence, adopting the modified technique, we have a simple recursive Adomian Algorithm for generating the individual terms of the series solution of Eqs. (8)–(10):

$$S_0 = s - \eta, \tag{20}$$

$$f_{1} = \frac{\alpha}{2}\eta^{2} + \left(\frac{\gamma}{1+\gamma}\right) \{(M^{2})L^{-1}(f_{o}') + 2L^{-1}A_{o} - L^{-1}B_{o}\}, \quad (21)$$

$$f_{k+1} = \left(\frac{\gamma}{1+\gamma}\right) \{(M^{2})L^{-1}(f_{k}') + 2L^{-1}A_{k} - L^{-1}B_{k}\}$$

$$\forall k = 1 \cdots n. \quad (22)$$

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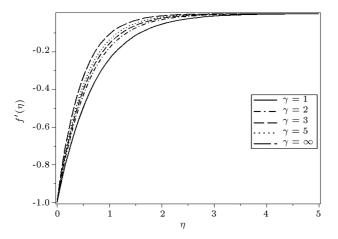


Figure 1: Shows the variation of velocity and boundary layer thickness for various values of Casson fluid parameter  $\gamma$  for s = 1 and M = 2.

For practical numerical computations, we shall use the finite *j*-term approximation of  $f(\eta)$ :

$$\phi_j(\eta) = \sum_{i=0}^{j-1} f_i.$$
(23)

The algorithm (20)–(22) is coded in the computer algebra package, Maple, and we employ Maple's built-in Padé approximants procedure. To achieve reasonable accuracy, we obtain the 41-term approximation of  $f(\eta)$ , i.e.  $\phi_{41}(\eta) = \sum_{i=0}^{40} f_i$ , where the first four terms are given as follows:

$$f_{0} = s - \eta, \qquad (24)$$

$$f_{1} = \frac{1}{2}\alpha\eta^{2} + \frac{1}{6}\frac{\gamma(-M^{2}+2)}{1+\gamma}\eta^{3}, \qquad (25)$$

$$f_{2} = -\frac{1}{6}\frac{\gamma s\alpha\eta^{3}}{1+\gamma} + \left(-\frac{1}{12}\frac{\gamma^{2}s}{(1+\gamma)^{2}} - \frac{1}{8}\frac{\gamma\alpha}{1+\gamma} + \frac{1}{24}\frac{\gamma M^{2}\alpha}{1+\gamma} + \frac{1}{24}\frac{\gamma^{2}sM^{2}}{(1+\gamma)^{2}}\right)\eta^{4} + \left(\frac{1}{30}\frac{\gamma^{2}M^{2}}{(1+\gamma)^{2}} - \frac{1}{30}\frac{\gamma^{2}}{(1+\gamma)^{2}} - \frac{1}{120}\frac{\gamma^{2}M^{4}}{(1+\gamma)^{2}}\right)\eta^{5}, \qquad (26)$$

$$f_{3} = \frac{1}{24} \frac{s^{2} \gamma^{2} \alpha \eta^{4}}{(1+\gamma)^{2}} + \left(\frac{1}{60} \frac{\gamma^{3} s^{2}}{(1+\gamma)^{3}} - \frac{1}{120} \frac{\gamma^{3} s^{2} M^{2}}{(1+\gamma)^{3}} + \frac{1}{40} \frac{\gamma \alpha^{2}}{1+\gamma} + \frac{1}{24} \frac{\gamma^{2} s \alpha}{(1+\gamma)^{2}} - \frac{1}{60} \frac{\gamma^{2} M^{2} s \alpha}{(1+\gamma)^{2}}\right) \eta^{5} + \left(\frac{19}{720} \frac{\gamma \alpha^{2}}{(1+\gamma)^{2}} - \frac{7}{20} \frac{\gamma^{3} s M^{2}}{(1+\gamma)^{3}} + \frac{1}{120} \frac{\gamma^{3} s}{(1+\gamma)^{3}} + \frac{1}{360} \frac{\gamma^{3} S M^{4}}{(1+\gamma)^{3}} - \frac{1}{60} \frac{\gamma^{2} M^{2} \alpha}{(1+\gamma)^{2}} + \frac{1}{720} \frac{\gamma M^{4} \alpha}{(1+\gamma)^{2}}\right) \eta^{6} + \left(-\frac{1}{5040} \frac{\gamma^{3} M^{4}}{(1+\gamma)^{3}} + \frac{1}{420} \frac{\gamma^{3} M^{2}}{(1+\gamma)^{3}} - \frac{1}{140} \frac{\gamma^{3} M^{2}}{(1+\gamma)^{3}} + \frac{2}{315} \frac{\gamma^{3}}{(1+\gamma)^{3}}\right) \eta^{7}.$$
 (27)

### 4. Results and discussion

In this section, we discuss the different physical parameters, such as fluid parameter  $\gamma$ , Hartmann number, M, and suction injection parameter s. Here, we use the diagonal Padè approximant for the valid convergent. Figure 1 shows that the

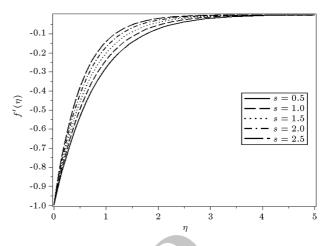


Figure 2: Shows the variation of velocity and boundary layer thickness for various values of shrinking parameter *s* for  $\gamma = 1$  and M = 2.

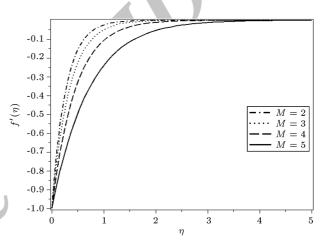


Figure 3: Shows the variation of velocity and boundary layer thickness for various values of Hartmann number *M* for s = 1 and  $\gamma = 3$ .

Table 1: Numerical values of $\alpha = f''(0)$ for $s = 1, M = 2$ and $\gamma = 1$ .		
Pade	α	
[5/5]	1.36569	
[10/10]	1.36668	
[15/15]	1.36668	
[20/20]	1.36668	
[25/25]	1.36668	

influence of fluid parameter  $\gamma$ . It shows that the magnitude of velocity and boundary layer thickness decreases with an increase in fluid parameter,  $\gamma$ . It is noticed that when the fluid parameter approaches infinity, the problem in the given case reduces to a Newtonian case. Figures 2 and 3 shows that the boundary layer thickens and the magnitude of the velocity decreases with an increase in Hartmann number, *M*, and suction injection parameter, *s*. Tables 1–3 gives the numerical values of  $\alpha = f''(0)$  for different order of approximations (Pade).

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Table 2: Numerical values of $\alpha = f''(0)$ for $s = 0.5, M = 2$ and $\gamma = 1$ .		
Pade	α	
[5/5]	1.215482	
[10/10]	1.215503	
[15/15]	1.215503	
[20/20]	1.215503	
[25/25]	1.215503	

Table 3: Numerical values of $\alpha = f''(0)$ for $s = 1, M = 3$ and $\gamma = 1$ .		
Pade α		

[5/5]	2.185549
[10/10]	2.184183
[15/15]	2.184183
[20/20]	2.184183
[25/25]	2.184183

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Sohail Nadeem obtained his Ph.D. degree from the Department of Mathematics at Quaid-i-Azam University, Pakistan, where he is working as Associate Professor. His fields of interest include: fluid dynamics, mathematical methods and nonlinear analysis.

Rizwan Ul Haq is currently a Ph.D. degree student in the Department of Mathematics at Quaid-i-Azam University, Pakistan. He is working on Newtonian and non-Newtonian shrinking and stretching sheet problems.

Changhoon Lee is working as Associate Professor in the Department of Computational Science and Engineering at Yonsei University, South Korea. His fields of interest include computational fluid dynamics.